2011 ARS, North America, San Diego

Track 1, Session 8

Begins at 1:00 PM, Wednesday, June 8th

Proving a New Refinery Design Using Reliability Throughput Modelling

Damien Willans SSR Engineering Pty Ltd





PRESENTATION SLIDES

The following presentation was delivered at the:

International Applied Reliability Symposium, North America June 7 - 9, 2011: San Diego, California

http://www.ARSymposium.org/2011/

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1.0 Introduction

- Damien Willans
- Director, SSR Engineering Pty Ltd
- Incorporated in 2009
- Key Highlights :
 - Specialize in reliability modeling
 - 15 to 20 years minerals processing design backgrounds for both company partners
 - Previously in-house reliability modelling, now consulting
 - Modelling software
 - SSR uses a flexible modeling platform Goldsim
 - Goldsim is a numerical analysis platform with a wide range of applications including engineering systems reliability.



Agenda

 1.0 Introduction 	5 min
 2.0 Modeling new projects 	5 min
 3.0 Case study - New project outline 	5 min
 4.0 Project setup – Client scope, data, 	
documents	10 min
 5.0 Producing the models 	10 min
 6.0 Model outputs and issues 	5 min
 7.0 Summary 	10 min
 Questions 	10 min

2.0 Modelling new projects

- Current Scenario
 - Resource demand and industry is booming.
 - Project scales have generated larger scale specialized engineering providers.
 - The larger they are, the harder it is to fully integrate all stages of project design and operations.
 - The path from resource ownership to fully functioning and integrated mine/processing facilities can be lengthy, expensive and rarely seamless.

2.0 Modelling new projects

- Engineering Construction Operation
 - Typically in Australia the major resource companies engage large engineering consultants to execute plant design.
 - The key criteria is project cost, combined with a performance guarantee.
 - Final design and construction is often handed off to large construction companies.
 - Plant is handed over to owner/operator for operations and maintenance.

Key point : The facility owner has limited opportunity to prove and optimise the design – particularly in the area of operations and maintenance effects.



3.0 Case study – New project outline

- Project outline
 - A relatively "new" player (in Alumina but not in resources).
 - Massive mine to raw product processing and port development.
 - Compelled to use publically available technology and engineering.
 - Utilizing a large engineering team with wide range of experience and design preferences.

3.0 Case study – New project outline

- Design process
 - Process flowsheet designed with final production number as starting point.
 - An assumed "operating" factor was then applied to get :
 - Final flowsheet data this was then used to size pumps, filters, piping etc.
 - Entire success of the plant process is dependent on the plant equipment meeting the assumed operating factor, not just initially but over time...



- Project definition stage is VERY important.
- 3 major requirements at model definition stage :
 - Client requirements
 - Data sourcing
 - Documentation and review



- 4.1 Client requirements
 - Initial requirement was a reliability "model" which had different meanings to each person.
 - My job was to show the potential outcomes from the models and how they could use them.
 - Significant demonstrations of the program (Goldsim) and explaining numerical analysis.
 - All expectations from owners, design engineers and operating partners were documented and updated during the project duration.



- 4.2 Data sourcing
 - Very critical to find/collate all available data and get agreement on its use.
 - Equally critical to assemble all of the data into a single source document for review by the client early in the modelling process.
 - For this project we required process flow diagrams (PFD's), equipment lists, area process descriptions, initial maintenance assumptions and failure data.
 - This (greenfield) project required some existing plant data from the operating partner.



Process Flow Diagrams Equipment list(s) Process Descriptions Operating Criteria Planned mtce freq. Failure data (statistics)

Create Model Design Criteria Docs

- Essential data comes together for 2 very important reasons :
- 1. Allows <u>alignment</u> of data and highlights <u>gaps</u>.
- 2. Eliminates uncertainty for those who only review the outcomes after modelling project essential completion.



- 4.3 Project documentation
 - Design criteria documents were then compiled for each process area.
 - These contained ALL relevant data to be used in each model (i.e., in one specific location).
 - Criteria generated significant "discussions" regarding some assumptions – a great tool.
 - Invaluable for project final model review stages when input data is often a point of contention (particularly for new players).



Overview

- 5.1 Starting with a plan
- 5.2 Building the models
- 5.3 Developing models the client can use
- 5.4 Building the combined (full-plant) model

- 5.1 Start with a plan
 - Start by breaking down total plant by areas.
 - Build a schedule for the overall project.
 - Create the modelling schedule based on model development stages – preliminary, area verification, combined model stage.
 - Update progress each week.



Build a schedule for the overall project.

Project Schedule		W	/k 1				۱	Wk	2				Vk∶						/k 4						'k 5					WI						Vk					Wk					Wk						k 1					Nk					Wk			
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- 5.2 Building the models
 - Start with a structure in mind.
 - Inputs Model Outputs
 - Input data includes :

o Process criteria, flowrates

o Equipment capacities (Nor / Max / Design)

o Operating rules

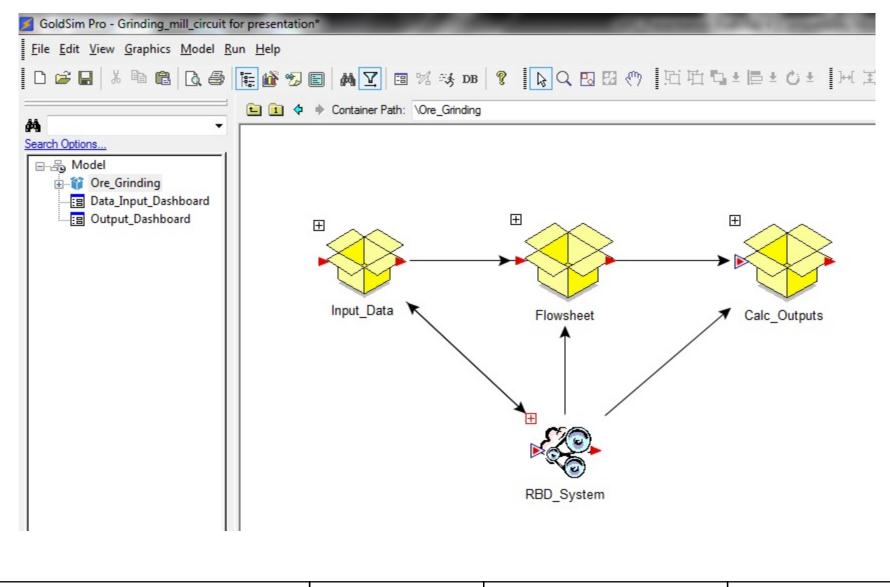
o Planned maintenance freq and durations

o Unplanned stoppages (failure data)

• Goldsim model architecture is flexible...

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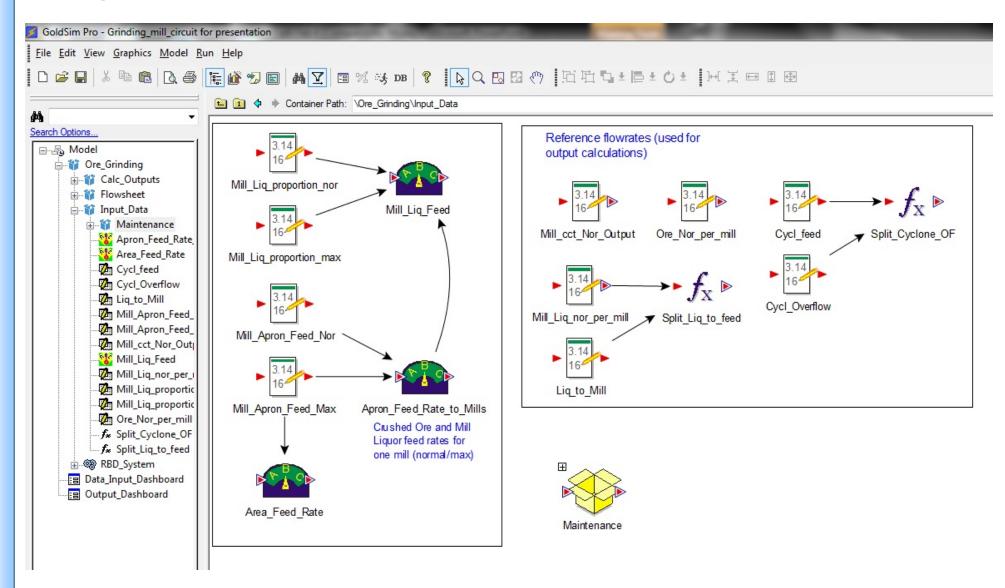
So consistent model structures are essential.



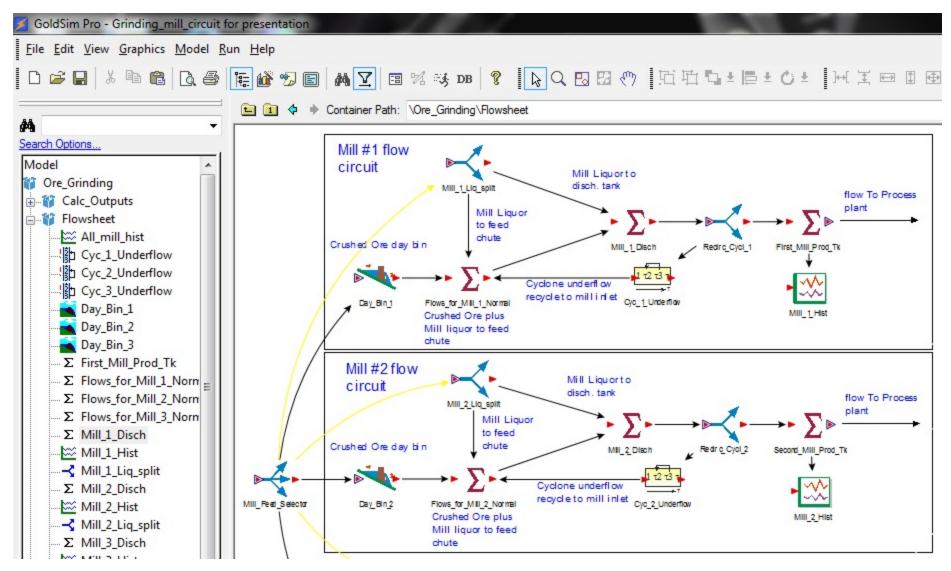
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Input data screen :



• Process flows :

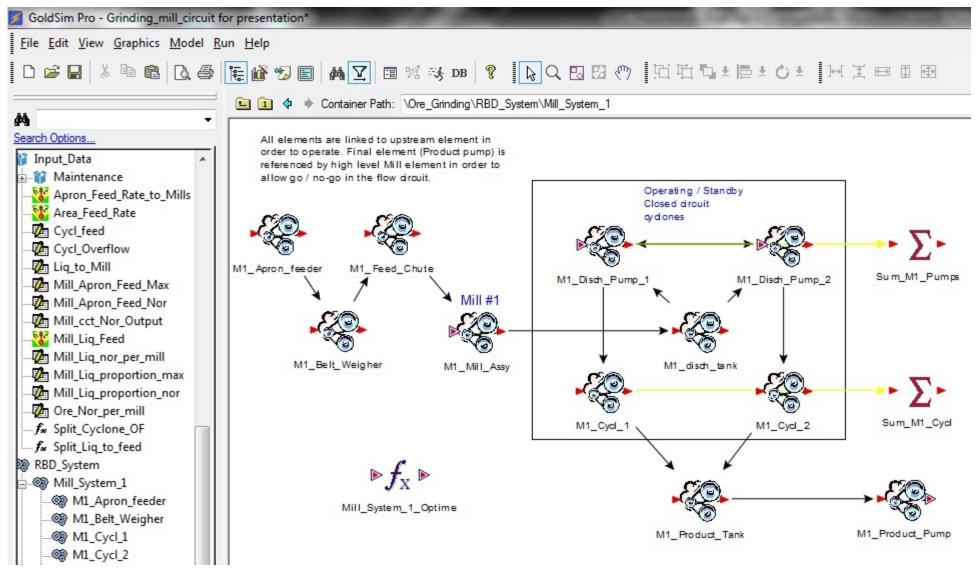


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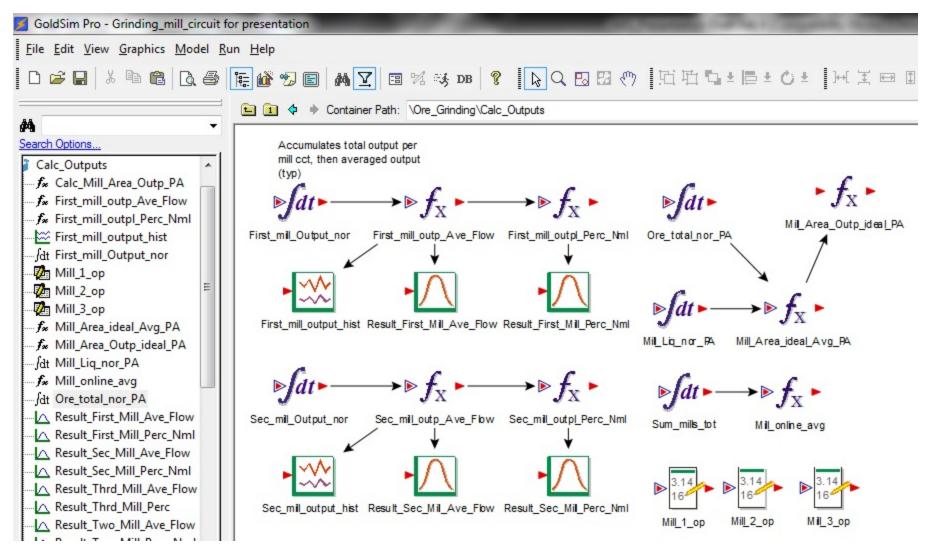
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• Reliability/Equipment elements :



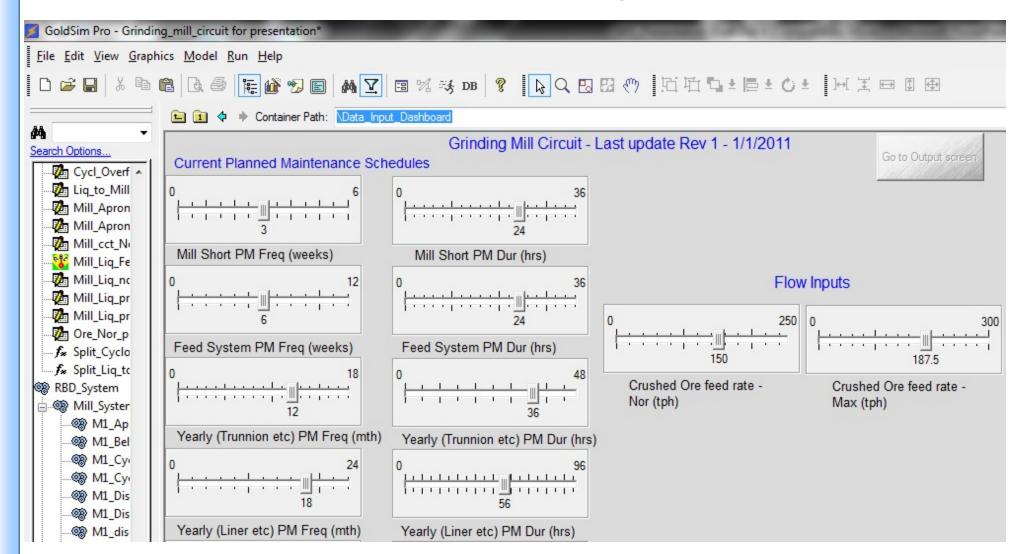
Calculated output screen :



- 5.3 Developing models the client can use
 - Goldsim uses dashboards for client model interface.
 - Line up inputs in design criteria <u>exactly</u> with model dashboards.
 - Discuss resultant model outcomes face to face.
 - Input/Output dashboards for this project included the Grinding area.



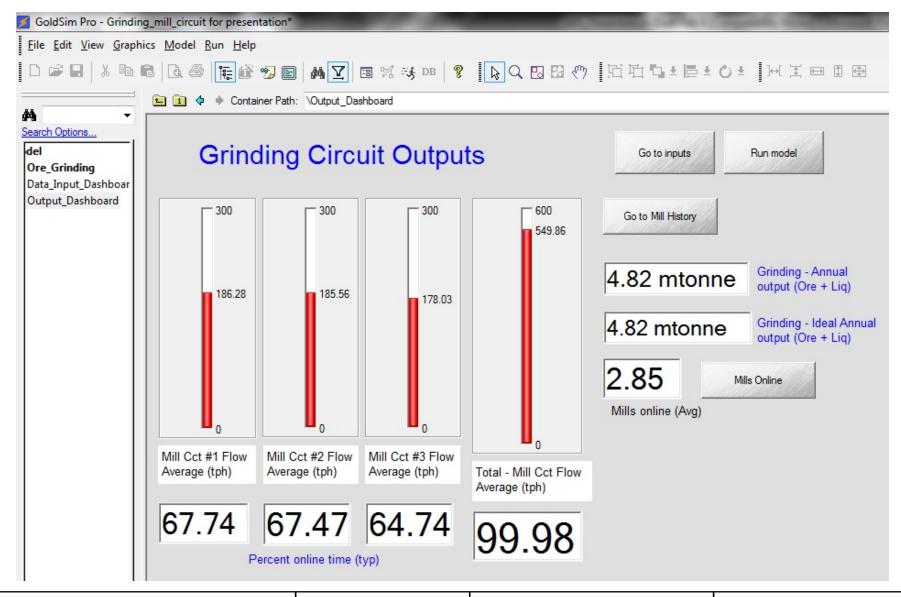
• Client model interface – model inputs :



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• Client model interface – model outputs :

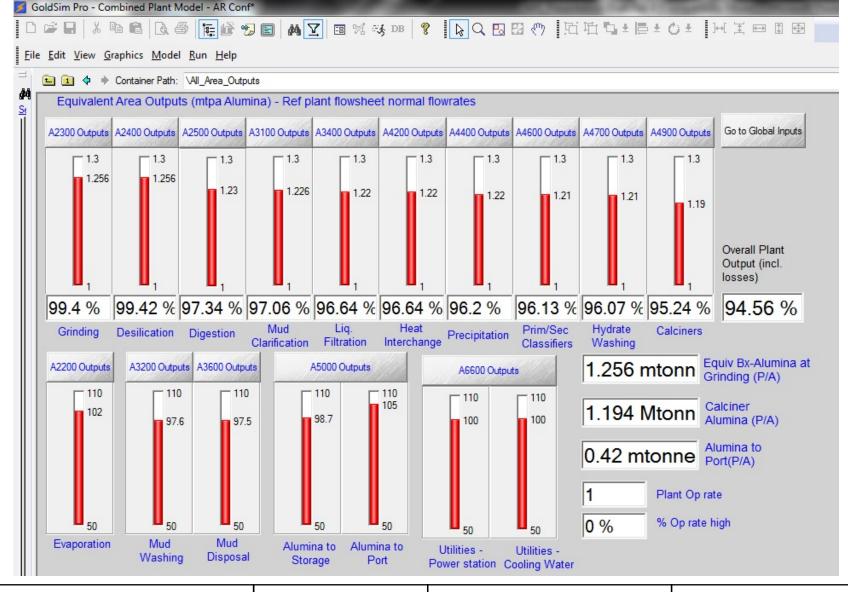


- 5.4 Building the combined plant model
 - Each area is built as a standalone model.
 - Utilise standard input/output formats.
 - Create a combined model by adding all process area models into one location.
 - Combined model simply connects inputs and outputs to provide a continuous circuit.
 - Important to re-evaluate operating and maintenance connections between areas (!!!)

Combined model assembly :

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Combined model – Overall Outputs :



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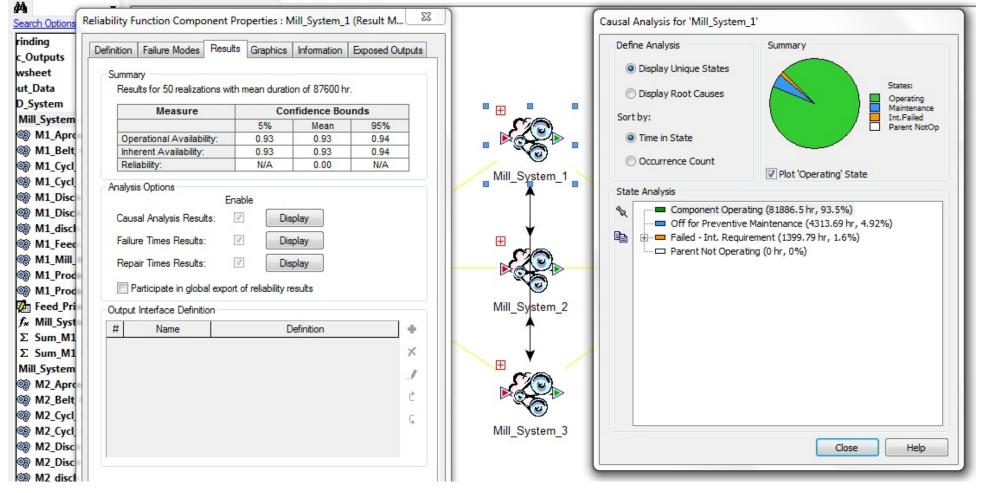
Combined model – System/Equipment analysis :

ź	GoldSim Pro - Grinding_mill_circuit*	

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Combined model – Bulk equipment analysis :

Model Description:

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of Realizations: 50

	Operat	ional Avai	lability	Inher	ent Availa	bility		Reliability		Mean Time to Failure	Mean Time to Repai
Element ID	5%	Mean	95%	5%	Mean	95%	5%	Mean	<u>95%</u>	hr	hr
Mill_System_1	0.934248	0.934778	0.935307	0.934248	0.934778	0.935307	N/A	0	N/A	590	10.0878
M1_Apron_feeder	0.934247	0.934777	0.935307	0.99895	0.999021	0.999092	N/A	0	N/A	13412.9	13.4362
M1_Belt_Weigher	0.934248	0.934778	0.935307	0.999962	0.999971	0.999979	N/A	0	N/A	102245	3.90662
M1_Cycl_1	0.92041	0.920934	0.921458	0.991477	0.99155	0.991624	N/A	0	N/A	698.136	5.92896
M1_Cycl_2	0.920412	0.920914	0.921415	0.991385	0.991462	0.991539	N/A	0	N/A	697.283	5.96856
M1_Disch_Pump_1	0.928648	0.929171	0.929694	0.994148	0.994247	0.994347	N/A	0	N/A	991.115	5.69697
M1_Disch_Pump_2	0.928696	0.929207	0.929718	0.994178	0.99427	0.994361	N/A	0	N/A	998.717	5.70289
M1_disch_tank	0.934248	0.934778	0.935307	1	1	1	N/A	0	N/A	103063	0.0898838
M1_Feed_Chute	0.934248	0.934778	0.935307	0.999537	0.999556	0.999574	N/A	0	N/A	8629.59	4.0102
M1_Mill_Assy	0.934242	0.934772	0.935303	0.990476	0.99099	0.991504	N/A	0	N/A	3179.18	27.0512
M1_Product_Pump	0.934248	0.934778	0.935307	0.994206	0.99429	0.994375	N/A	0	N/A	991.191	5.64851
M1_Product_Tank	0.934248	0.934778	0.935307	1	1	1	N/A	0	N/A	102393	0.0985797
Mill_System_2	0.934228	0.93474	0.935251	0.934228	0.93474	0.935251	N/A	0	N/A	585.442	10.1122
M2_Apron_feeder	0.934228	0.934739	0.935251	0.999015	0.999095	0.999175	N/A	0	N/A	13764.1	12.7041
M2_Belt_Weigher	0.934228	0.93474	0.935251	0.999956	0.999967	0.999978	N/A	0	N/A	97608.4	4.0137
M2_Cycl_1	0.92048	0.92098	0.92148	0.991463	0.991536	0.99161	N/A	0	N/A	699.077	5.9465
M2_Cycl_2	0.92045	0.920957	0.921463	0.991508	0.991586	0.991665	N/A	0	N/A	704.517	5.96399
M2_Disch_Pump_1	0.928706	0.929205	0.929705	0.994201	0.994282	0.994363	N/A	0	N/A	996.975	5.67152
M2_Disch_Pump_2	0.928632	0.929138	0.929644	0.994156	0.994235	0.994315	N/A	0	N/A	988.513	5.67689
M2_disch_tank	0.934228	0.93474	0.935251	1	1	1	N/A	0	N/A	108461	0.102898
M2_Feed_Chute	0.934228	0.93474	0.935251	0.999539	0.999557	0.999574	N/A	0	N/A	8512.74	3.91783
M2_Mill_Assy	0.934223	0.934734	0.935246	0.99044	0.990887	0.991335	N/A	0	N/A	3128.15	27.2402
M2_Product_Pump	0.934228	0.93474	0.935251	0.994137	0.994224	0.994312	N/A	0	N/A	986.68	5.67177
M2_Product_Tank	0.934228	0.93474	0.935251	1	1	1	N/A	0	N/A	102965	0.103303
Mill System 3	0.934098	0.934553	0.935008	0.934098	0.934553	0.935008	N/A	0	N/A	579.995	10.19

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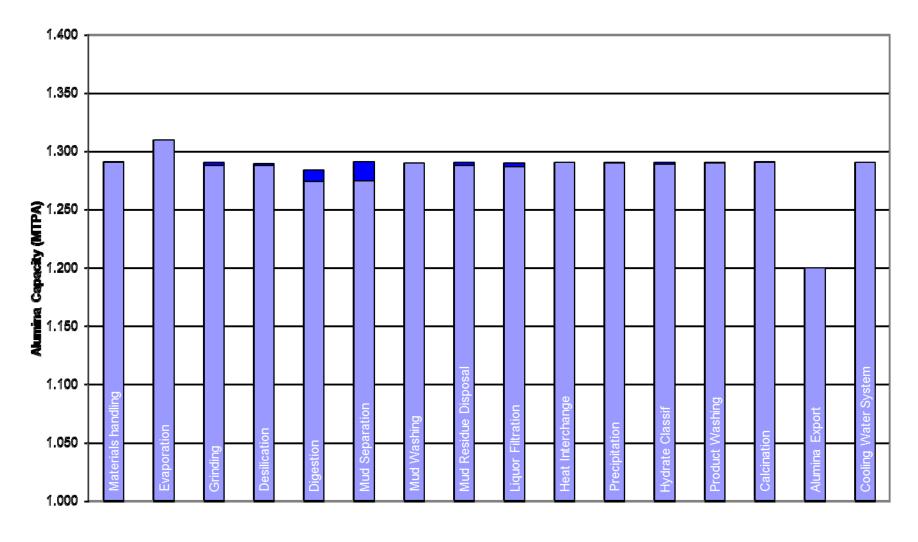
- 6.1 Project requirements
 - Phased development client is always confident of outcomes at each project milestone (no black box !!).
 - Use <u>agreed</u> inputs via reviewed design criteria.
 - Determine all model scenarios to be evaluated.
 - Present findings with a wider audience in mind (visual comparisons rather than just numbers).

- Multiple model scenario investigations :
 - S1 Evaluate baseline operating and maintenance criteria using initial design.
 o Look for areas with largest production shortfall and identify causes (Ops / Mtce / Design?).
 - S2 Examine initial design assumptions redundancy.

- Multiple model scenario investigations :
 - S3 Case studies included minimum level of equipment (i.e., no spares) to show where they are really needed.
 - S4 Ran area and combined models both with and without failure modes to show both sensitivity (to failures) and plant potential in ideal conditions.

Model Results – by Area – as designed :

Area Alumina Capacity - Fall Data + No Fall Data - Equiv Alumina mtpa



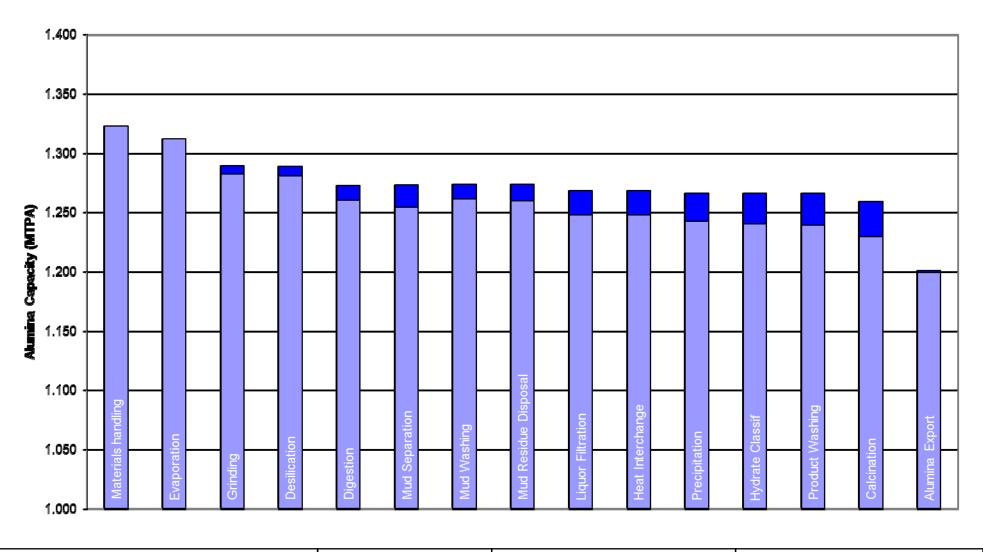
• Model Results – by Area – minimum asset case :

1.400 1.350 1.300 1.250 1.200 **X1**.150 **1**.100 A 1.050 Water System Materials handling Washing Disposal Filtration Evaporation Precipitation Calcination 8 Classif ള1.000 Washing Export Separation Grinding Mud **2**0.950 Residue Digestion Liquor Hydrate Cooling Alumina Interchange Product Mud 0.900 Mud 0.850 Heat Desilication 0.800 0.750 0.700

Area Capacity - minimum asset case - Equiv Alumina - (mtpa)

Model Results – Combined Output :

Plant Alumina Capacity - Fall Data + No Fall Data - Equiv Alumina mtpa (10Yr dur)



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- Case Study project outcomes
 - Clear definition and alignment of design data was achieved before detailed design process.
 - Proved the design engineer's operating factor assumption was exceeded (for given criteria!).
 - Provided a statistical basis for the plant design capacity for the client's project cost estimate.



- Case Study project outcomes
 - Also showed several process areas where value improvements could be investigated.
 - Client now has a tool to validate further maintenance strategy inputs vs. plant capacity.



- Capacity modelling vs. project stages
 - Early adoption (Feasibility/Study stage) Capital savings through optimizing equipment capacities and redundancy.
 - During Design (Prelim/Basic engineering) Value engineering processes, confirming effects of maintenance and operating strategies on adopted design.



- Capacity modelling vs. project stages
 - Detailed Engineering and construction Use to refine and verify maintenance strategy development processes (e.g., RCM). Also provide initial resourcing estimates for labour, commodities (spares) etc.
 - After Startup Verify model vs. plant outputs, then use for both capital and maintenance program validation.



- Value adding
 - Resourcing Run the models to gauge resource requirements for varying strategies (labour, spares, commodities etc).
 - Energy Energy use is time and condition related – so can be built into these models (e.g., pump efficiency vs. changeout freq).
 - Model company wide operational and mtce initiatives across multiple facility models before making the change (!).



Where to Get More Information

- Web links
- www.ssr-eng.com
- www.goldsim.com
- E-mail : <u>damien@ssr-eng.com</u>
- or : info@ssr-eng.com





Thank you for your attention ③

Do you have any questions?

